



| ••••• | مجوز: | شماره |
|-------|-------|-------|
|-------|-------|-------|

## «آگهی ارزیابی کیفی تامینکنندگان»

شرکت پالایش نفت امام خمینی (ره) شازند در نظر دارد کالاهای موضوع بند «یک» آگهی حاضر را از طریق برگزاری مناقصه عمومی دو مرحلهای از تامین کننده واجد شرایط خریداری و تامین نماید.

## 1) موضوع مناقصه

## الف) شرح مختصر كالا

| مبلغ تضمین شرکت در<br>فرآیند ارجاع کار (ریال) | بر آورد هزینه<br>انجام موضوع مناقصه (ریال) | مقدار/تعداد | شرح مختصر كالا         | شماره مناقصه                     | رديف |
|---|--|-------------|------------------------|----------------------------------|------|
| ۳۰,۲۰۰,۰۰۰,۰۰۰                                | 1,880,000,000                              | 64 متر مكعب | كاتاليست ايزومريزاسيون | RND-9818225-MY<br>(تجديد مناقصه) | ١.   |

#### ب) شرايط اوليه متقاضي

- ۱- داشتن شخصیت حقوقی، شماره اقتصادی، توانایی مالی، سابقه کار مفید و مرتبط با موضوع مناقصه.
  - ۲- داشتن کد ملی/شناسه ملی جهت شرکت در مناقصه الزامی است.
- ٣- داشتن حسن سابقه و ارائه گواهينامههاي مورد نظر از خريداران قبلي و اعلام اسامي خريداران قبلي در صورت لزوم.
- ۴- توانائی ارائه تضمین شرکت در فرآیند ارجاع کار (در صورت تائید در ارزیابی کیفی مناقصه گران) و همچنین تضمین انجام تعهدات (در صورت برنده شدن در مناقصه) مطابق آئیننامه تضمین برای معاملات دولتی موضوع تصویبنامه هیأت وزیران به شماره ۱۲۲۴۰۲/ت مورخ ۱۳۹۴/۰۹/۲۲.
- △ داشتن صورتهای مالی حسابرسی شده توسط سازمان حسابرسی یا اعضاء جامعه حسابداران رسمی، مطابق بـا مـاده ۲ آیـیننامـه راهکارهـای افـزایش ضـمانت اجرائـی و تقویـت حسابرسی، جهت مناقصه ردیف «۱» الزامی میباشد.

#### 2) نام و نشانی دستگاه مناقصهگزار

شرکت پالایش نفت امام خمینی (ره) شازند واقع در استان مرکزی، اراک- کیلومتر ۲۰ جاده بروجرد.

#### **3) مهلت و محل دریافت فرمهای استعلام ارزیابی کیفی**

متقاضیانی که دارای شیرایط اولییه (بنید ب) بیوده و آمیادگی لازم جهیت انجیام مناقصیه میذکور را دارنید می تواننید پیس از انتشیار آگهی نوبت دوم (۳ روز پس از انتشار آگهی نوبت اول) به مدت ۵ روز گاری ضمن ارسال تقاضای شرکت در مناقصه مورد نظر از طریق نمیابر ۳۳۶۷۲۰۱۳–۰۸۶ و ۴۶۲۳۶۶۰ و ۴۶۲۳۶۶۰ دریافت و بر اساس آن مدارک لازمه را تکمیل و صرفاً بر روی لوح کشرده (CD) به این شرکت تحویل یا ارسال نمایند.

#### 4) زمان و محل تحویل اسناد ارزیابی کیفی (تکمیل شده توسط متقاضیان)

زمان تحویل اسناد ارزیابی کیفی توسط مناقصه گران، ۲ هفته پس از آخرین مهلت ارسال تقاضای شرکت درمناقصه میباشد. ضمناً محل تحویل یا ارسال لوح فشرده (CD) حاوی فرمها و مدارک تکمیل شده، به نشانی اراک کیلومتر ۲۰ جاده بروجرد سه راهی شازند - شرکت پالایش نفت امام خمینی (ره) شازند - اداره تدارکات و امور کالا حساختمان ب - طبقه همکف اتاق ۱۲۱ - کدپستی ۱۹۱۱ - ۱۹۶۳ - ۱۹۶۳ - ۱۹۶۳ - ۱۹۶۳ - ۱۹۶۳ میباشد. بدیهی است به مدارک ارسالی بعد از مهلت مقرر ترتیب اثر داده نخواهد شد ضمناً دادن پیشنهاد و ارائه اسناد و مدارک هیچگونه حقی برای متقاضی ایجاد نمی کند. لازم بذکر است دستگاه مناقصه گزار پس از وصول لوح فشرده حاوی اسناد ارزیابی کیفی ظرف مدت ۱ ماه نسبت به اعلام اسامی واجدین شرایط اقدام خواهد نمود.

توجه: مناقصه گران نخست با مراجعه به سایت این شرکت (همزمان با انتشار آگهی نوبت دوم) میبایست ۲ برگ فرم ارزیابی کیفی را اخذ و پس از تکمیل به همراه مدارک مربوطه، صوفاً بر روی لوح فشرده (CD) درج و در موعد مقرر به آدرس این شرکت ارسال یا تحویل نمایند، این شرکت نیز پس از ارزیابی کیفی متقاضیان، از شرکتهایی که حداقل امتیاز قابل قبول را کسب نموده باشند، جهت دریافت اسناد مناقصه دعوت بعمل خواهد آورد.

توصیه: پیشنهاد میگردد شرکتهای متقاضی در اسرع وقت نسبت به ثبت نام در سامانه تامین الکترونیکی کالای نفت (EP) اقدام نمایند.

روابط عمومي شركت پالايش نفت امام خميني (ره) شازند

أدرس اينترنتي: WWW.IKORC.IR

# چاپ اول : تاریخ ۸۹/۰۸/۲۸ روزنامه اطلاعات چاپ دوم: تاریخ ۹۹/۰۹/۰۲ روزنامه اطلاعات

 آخرین مهلت اعلام آمادگی توسط فاکس تا تاریخ ۹۹/۰۹/۰۸ میباشد و متعاقباً شرکتهایی که اعلام آمادگی نمودند تا پایان وقت اداری روز دوشنبه مورخ ۹۹/۰۹/۲۴ مهلت دارند CD ارزیابی کیفی را بر اساس مدارک پیوست تحویل نمایند.



# شركت بالايش نفت امام خميني (ره) شازند (سهامي عام)

# شركت /فروشگاه محترم ...... مناقصه عمومي دو مرحلهاي شماره: RND-9818225-MY

لطفاً به منظور انجام ارزیابی کیفی آن شرکت / فروشگاه ، طبق جداول ومحاسبات پیوست مدارک ومستندات ذیل را ارائه فرمایید:

# 1- جهت ارزيابي توان مالي

الف : مدارک مورد نیاز جهت ارزیابی حداقل یکی از موارد ذیل:

١-الف : ماليات متوسط سالانه پرداخت شده (برگ تشخيص/ قطعي ماليات عملكرد پنج ساله اخير)

٢-الف : فروش يكسال گذشته (ليست خريداران شامل نام خريدار ،شرح كالا،مبلغ كالا)

٣-الف: اظهار نامه مالياتي

۴ الف : حداكثر تائيديه كتبي اعتبار از طرف بانكها

۵-الف :دارائیهای ثابت

٤-الف متوسط بيمه سالانه

۷-الف صورتهای مالی حسابرسی شده توسط سازمان حسابرسی یا موسسات حسابرسی مورد تائید

تبصره : ارائه صورتهای مالی حسابرسی شده (بند ۷- الف) در خصوص معاملاتی کـه مبلـغ آن بـیش از ۱۰ برابـر نصـاب معاملات متوسط باشد الزامیست .

# ب: نحوه ارزیابی و امتیاز دهی توان مالی :

(ماليات متوسط سالانه×100 / فروش يك سال كذشته / تأثيديه كتبي اعتبار بانكي )-RI رود= ES

| امتياز | فرمول                          |
|--------|--------------------------------|
| 1      | . <b>\/Y</b> ×ES≤RJ            |
| 9.     | ES≤RI < <b>1/∀</b> ×ES         |
| ۸۰     | ./∧×ES≤RI <es< th=""></es<>    |
| ٧٠     | ./\$× ES≤ RI <./ <b>^</b> × ES |
| ۶٠     | RI <₁/タ ×ES                    |

# ٢- جهت ارزيابي حَسن سابقه / مشتريان قبلي / تضمين كيفيت و تضمين خدمات محصولات مدارك ذيل مورد نياز است :

الف: کیفیت کالای مورد نظر ( ارائه مدارکی مبنی بر فروش کالای مورد نظر به خریداران ارائه مدارکی مبنی بر تطابق مشخصات فنی ارائه شده از سوی فروشنده با کالای مورد نظر )

ب: ارائه استانداردها وگواهی تضمین کیفیت ساخت کالای مورد نظر فروخته شده ( در صورت موجود بودن )

ج: ارائه مدارک مربوطه در خصوص دارا بودن نمایندگی

د : ارائه تائیدیه کالای فروخته شده

# ٣- جهت ارزیابي تجربي مدارک ذیل مورد نیاز است:

الف: ارائه اساسنامه شرکت یا پروانه کسب

ب: ارائه شماره اقتصادی / کد ملی

The same of the sa

تاريخ:

شركت يالايش نفت امام خميني ( ره ) شازند ( سهامي عام )

فرم ارزيابي كيفي تأمين كنندكان المكرَّ تَحْرَكُونَ الْمُورِكُونِ كَالا

مناقصه عمومي دو مرحله اي شماره: RND-9818225-MY نام شركت: تحت عنوان: خريد كاتاليست ايزوم يزاسيون

|                                     | O3:3:3-33:::                           |                          |                                | ,  |               |                |                  |             |
|-------------------------------------|--|--------------------------|--------------------------------|--|---------------|----------------|------------------|-------------|
| A : توان مالی<br>ارزبایی بر اساس یک | نی از پارامترهای <b>ذیل انجام می ش</b> | ئىود:                    |                                |  |               |                |                  |             |
|                                     | فروش سالانه                            | 1                        | هار نامه مالیا                 |  |               | متوسط مالياه   | ت سالانه         |             |
| <br>] دارائی ه                      |  |                          | ید کتبی اعتب                   |  | <b>=</b>      | متوسط بيمه س   |                  |             |
|                                     |  |                          | 7                              |  |               | ا متوسط بيمه س |                  |             |
| ا صورتهای                           | <b>، مالی حسابرسی شده: دارد</b>        | ، ∟ ندا                  | ارد                            | سیزان توان م <b>ال</b> ہ                         |               |                | ميا              | يليارد ريال |
| امتياز كسب ش                        |  | ۶۰                       | y. 🗹                           | ۸۰ 🗆   | ]             | <b>٩٠</b> [    | 1                |             |
| حداقل امتيازلازم:                   | V-                                     |                          |                                |  |               |                |                  |             |
| B : ارزیابی مشت                     | ریان قبلی ، حسن سابقه وتض              | سمين كيفي                | ت وخدمات                       | حصولات   |               |                |                  |             |
| پارامترهای ارزیاب                   | <i>.</i>                               |                          | عالی<br>امتیاز۵                | بسیار ۴  | فوب<br>امتیاز | خوب<br>از۳     | مورد تأیی ن<br>⊶ | نیست        |
| کیفیت کالای مورد                    | د نظر مندرج در اسناد فنی ارا           | ائه شده                  | *                              |  |               |                |                  |             |
| خدمات وپشتیبانی                     | •                                      |                          |                                | *  |               |                |                  |             |
| انجام تعهدات(کار                    | ِانتى)                                 |                          |                                | *  |               |                |                  |             |
| ظرفیت تولید                         |  |                          |                                |  |               |                |                  |             |
| توان تجهیزاتی<br>امتیاز /           |  |                          |                                |  | 14            | \ - 2/         | - (              |             |
|                                     |  | <del></del>              |                                | <b>P</b>   | ,,,,,,        | ( 2/           | -10/X            | 94:         |
| C : ارزیابی تجرب                    | ن                                      | سال                      | نأسيس:                         |  |               |                |                  |             |
|                                     |  |                          | سابة                           |  | امتياز        |                |                  |             |
|                                     |  | با بیث                   | ں از ۱۰ سال                    | ابقه   | 1             | -              |                  |             |
|                                     | تولید کننده/سازنده کالا                | ۱۵                       | ل تا ۱۰ سال،                   | ابقه   | ٩٠            |                |                  |             |
|                                     |  |                          | نر از ۵ سال                    | <del> </del>                                     | ٨٠            | _              |                  |             |
|                                     | تأمين كننده كالا                       |                          | <u>ں از ۱۰ سال</u>             | <del> </del>                                     | ۸٠            | 1              |                  |             |
|                                     | حسد السام الم                          |                          | ل تا 10 سال ،<br>نر از ۵ سال ، | <del>                                     </del> | ۶۰ 🛠          |                | •                |             |
| _ <br> متياز سازنده كالا            | :                                      |                          | <u> </u>                       | 1  |               | Ĺ              |                  |             |
| امتيازتامين كننده كا                | ٤: ٢٠                                  |                          |                                |  |               |                |                  |             |
| بر اساس ارزیابی مد                  | ارک فوق شرکت مذکور مورد آ              | تائید می با              | اشد                            | اولويت معيار                                     | : 6           |                | ζ' A             | Υ'          |
| به دلیل عدم ارائه م <b>ا</b>        |  | رد تائید نم <sub>و</sub> | ی باشد                         |  |               |                | В                | 1           |
| ١- عدم ارائه                        | مدارک مالی                             |                          |                                | 0  | - 14          |                | ۲ C              |             |
|                                     | مدارک حسن سابقه و                      |                          |                                | فرمول کا   | +/1           | 4+C)           | 1 = / Y · (/     | امتياز كل   |
| ۲- عدم ارائه                        | مدارک تجربه و سوابق مربوط              |                          |                                | ا <b>متیاریسازنده/تو</b><br>امتیازتامین کننده    | ·10:0000-50   | zyle.          | "8+17            | 11+1        |
|                                     | /                                      |                          | ,                              |  |               |                |                  | 1           |

# مشخصات فني و اطلاعات مربوطه:

| مقدار درخواستی | واحد كالا | شرح کالا               | رديف |
|----------------|-----------|------------------------|------|
| 64             | М3        | ISOMERIZATION CATALYST | 1    |

# اطلاعات تكميلى پيوست مى باشد..

۱- کاتالیست میبایست در بشکه های فلزی نو و استاندارد و بروی پالت تحویل گردد.

۲- فروشنده موظف است همزمان با بررسی پیشنهادات فنی، مقدار یک کیلوگرم از کاتالیست پیشنهادی خود را بعنوان نمونه کالا جهت انجام تست پایلوت در پژوهشگاه صنعت نفت و ... ارائه نماید و هزینه های تست پایلوت و ... بعهده فروشنده می باشد، همچنین شرکت برنده متعهد می گردد با یکی از شرکتهای مورد تایید وزارت نفت برای انجام بازرسی های مورد نیاز و نمونه برداری ازخط تولید جهت تست های فیزیکی و شیمیایی مطابق با DATA SHEET سازنده کاتالیست قرارداد منعقد نماید که هزینه مربوطه بعهده فروشنده می باشد و میبایست مقدار یک کیلوگرم نمونه کاتالیست خط تولید نیز بمنظور بررسیهای مجدد در پژوهشگاه صنعت نفت ارسال که هزینه بررسی در پژوهشگاه صنعت نفت بعهده پالایشگاه می باشد.

# Technical Specifications of ISOMERIZATION Catalyst « RND-9818225-MY»

- 1. Definition
- 2. Introduction
- 3. Prequalification Criteria
- 4. Process Description
- 5. Feed and products Specification
- 6. Catalyst Performance
- 7. Operating Constraints
- 8. Scope of Services
- 9. Evaluation Criteria
- 10. Guarantees
- 11. Penalties

## **Section 1: Definition**

- 1. **Buyer**: shall mean Imam Khomeini Oil Refining Co. (hereinafter referred as IKORC), incorporated and existing under the laws at Islamic Republic of Iran is located at 20Km.BroojerdRoad-Arak-Iran.
- **2. Supplier**: shall mean any supplier/vendor who shall be responsible for supply catalyst.
- 3. ISOM: Isomerization unit is designed to process Light Naphtha received from the Naphtha Splitter in NHT2 to improve RON of light naphtha employing platinum catalyst to convert low quality light naphtha in the presence of hydrogen. The unit is designed for a capacity of 8500 BPSD of low octane hydrotreated light naphtha.
- 4. **Purchase order, P.O** means the binding agreement between buyer and catalyst supplier for the supply of Isomerization atalyst and additional services as described in the "Purchase order documents".

### **Section 2: Introduction**

The technical specification is being released for procurement of suitable catalysts for Isomerization Unit (ISOM) of Imam Khomeini Oil Refining Company. The feed basis, terms of reference, product yields & qualities, general description, constraints definition, scope of supply & services, performance guarantees and penalties etc. follow in the subsequent sections of the document.

The Product quality and yield pattern and RON of Isomerate to be submitted with the technical bid.

Imam Khomeini Oil Refining Company (IKORC) require 60 m<sup>3</sup> of catalyst for Isomerization unit (ISOM), which was originally designed and licensed by RIPI (Research Institute of Petroleum Industry) with one reactor to process 8500\*\* BBL/day of Light Naphtha and guaranteed Isomerate product RON(RON= Min. 86).

Bidders are required to submit 1 KG sample of Main/Active Catalyst to IKORC. The sample is required to be submitted before the due date of tender. Offer, without the sample is liable to be rejected.

\*\*This amount of feed is based on design condition of the unit.RON & yield of the product for minimum 80 m³/h (12076 BBL/day)should be calculated and guaranteed by catalyst suppliers.

# **Section 3: Pre Qualification Criteria (PQC)**

- 1. The bidder should be original manufacturer of Catalysts for ISOM unit or official local agent and have supplied the catalyst anywhere in the world from 2015 onwards for ISOM unit with same type of catalyst.
- 2. The catalyst supplier shall provide references regarding successful and satisfactory performance of the offered same type of catalyst for the desired ISOM. units operating under similar conditions and same or better guaranteed performance in Iran or abroad. The reference catalyst must have completed minimum one year of successful operation. Reference details including the copy of the purchase order to be attached. Offers, without any reference of same type of catalyst are liable to be rejected.
- 3. IKORC may at its discretion seek the performance details of the supplier's catalyst(s) from end users with similar plants who are using the same catalyst(s), which is offered to IKORC. In the event of receipt of no satisfactory performance, the catalyst(s) offered will deem

to be technically disqualified and this offer will not be considered for further evaluation.

## **Section 4: Process Description**

Isomerization unit is designed to process Light Naphtha received from the Naphtha Splitter in NHT2 to improve RON of light naphtha. Unit design capacity is 8500 BPSD. The unit turndown ratio is 50% of the

There are two primary products from the unit:

- Isomerate routed to product storage.
- Stabilized LPG routed to product storage.

There are additionally:

design capacity.

• Stabilizer Deethanizer off Gas directly routed to the refinery fuel gas header.

ISOM consists of the following sections:

- (a) Reactor Section
- (b) Separation Section
- (c) Make -up hydrogen compressor.

Section 5: Feed and ProductsSpecification

**5-1-1 Feed Specification** 

a-FreshFeed

The feedstocks of ISOM Reactor are Light Naphtha from the Naphtha Splitter in NHT2 and NC6 Recycle from Deisohexanizer column (Table 1, 2). Make-up hydrogen supplied from Octanizing and GHT Units (Table 3).

| Table 1 -PROPERTIES OF ISOMERIZATION FRESH FEED * |                         |              |  |
|---|-------------------------|--------------|--|
| Source: Naphtha hydro treatin                     | g unit (NHT2)           |              |  |
| Composition Data wt%                              | <b>Design Condition</b> | Actual Run** |  |
| N-C4  | 0                       | 0.01         |  |
| N- pentane  | 0                       | 3.02         |  |
| Isopentane  | 8.82                    | 10.82        |  |
| N-C5  | 15.02                   | 17.23        |  |
| 2,2DMC4   | 4.15                    | 0.32         |  |
| CC5   | 5.63                    | 1.47         |  |
| 2,3DMC4   | 3.67                    | 1.48         |  |
| 2MC5  | 8.02                    | 9.61         |  |
| 3MC5  | 4.95                    | 7.29         |  |
| N-C6  | 18.27                   | 17.85        |  |
| 2,2DMC5   | 1.13                    | 0.23         |  |
| MCC5  | 13.89                   | 5.52         |  |
| 2,4DMC5   | 0.43                    | 0.68         |  |
| 2,2,3TMC4   | 0                       | 0.02         |  |
| Benzene   | 5.7***                  | 2.27         |  |
| 3,3DMC5   | 0.06                    | 0.15         |  |
| CC6   | 9.88                    | 4.07         |  |
| 2MC6  | 0.29                    | 3.80         |  |
| 2,3DMC5   | 0.02                    | 1.63         |  |
| 1,1DMCC5  | 0                       | 0.39         |  |
| 3MC6  | 0.07                    | 4.14         |  |
| cis-1,3DMCC5                                      | 0                       | 0.92         |  |
| trans-1,3DMCC5                                    | 0                       | 0.77         |  |
| 3EC5  | 0                       | 0.32         |  |
| Trance-1,2DMCC5                                   | 0                       | 1.52         |  |
| N-C7  | 0                       | 2.97         |  |
| MCC6  | 0                       | 0.89         |  |
| EthylCC5  | 0                       | 0.07         |  |
| Toluene   | 0                       | 0.49         |  |
| Total   | 100                     | 99.95        |  |
| N-Paraffins                                       | 33.29                   | 38.06        |  |

| Isoparaffins                |                | 31.18  | 42.65   |
|-----------------------------|----------------|--------|---------|
| Aromatics                   |                | 5.7    | 2.75    |
| Naphthenes                  |                | 29.4   | 15.63   |
| Olefins                     |                | 0.43   | 0.90    |
| Total                       |                | 100    | 100     |
|                             | IBP            | •••    | 45      |
|                             | 5%             | •••    | 49      |
|                             | 10%            | •••    | 52      |
| Distillation                | 30%            | •••    | 57      |
| Range,                      | 50%            | •••    | 61      |
| ASTM D- 86                  | 70%            | •••    | 65      |
|                             | 90%            | •••    | 71      |
|                             | 95%            | •••    | 75      |
|                             | FBP            | •••    | 85      |
| Total Sp. Gr                |                | 0.691  | 0.673   |
| Molecular W                 | eight, kg/kmol | 80.76  |         |
| Total Sulfur, ppm wt        |                | <0.5   | 0.41    |
| Total Nitrogen, ppm wt      |                | <0.1   | 0.5     |
| Viscosity, cP               |                | 0.2681 |         |
| Water ppm                   |                | •••    | 20      |
| STD Volume Flow Rate, m3/hr |                | 56.31  | 80.0 ** |

\*\* RON & yield of the product for minimum 80 m³/h(12076 BBL/day)should be calculated and guaranteed by catalyst suppliers.(All calculation and guaranties must be based on the actual unit conditions including the amount of feed and its components)

\*\*\* Benzene content of the product should be calculated and guaranteed by catalyst suppliers based on the fresh feed's benzene content of design condition (5.7 wt%).

# b- NC6 Recycle

| Table 2- NC6 Recycle from Deisohexanizer column * |             |             |  |
|---|-------------|-------------|--|
| Item  | Design Data | Actual Data |  |
| Tem. °C   | 96          | 97          |  |
| Pressure, Barg                                    | 28.4        | 28          |  |
| Total mass flow ,Kg/hr                            | 34658       | -           |  |
| Molecular Weight, kg/kmol                         | 85.55       | -           |  |
| STD Volume Flow Rate, m <sup>3</sup> /hr          | 50.12       | 20          |  |
| Composition, wt%                                  |             |             |  |
| Cycloheptane                                      | 0.011332    | 0           |  |
| 22-Mbutane  | 1.009532    | 0           |  |
| 23-Mbutane  | 3.926236    | 0.34        |  |
| 2-Mpentane  | 21.02612    | 4.48        |  |
| 3-Mpentane  | 22.0655     | 10.51       |  |
| N-Hexane  | 21.36678    | 37.07       |  |
| 2,2-Dimethylpentane                               | -           | 0.55        |  |
| Mcyclopentan                                      | 25.35456    | 33.06       |  |
| 2,4-Dimethylpentane                               | 0           | 0.56        |  |
| Benzene   | 0.004507    | 0           |  |
| Cyclohexane                                       | 5.235436    | 5.95        |  |
| C7+   | 0           | 7.48        |  |
| Total   | 100         | 100         |  |

# 5-1-2 Make Up Hydrogen

The make-up hydrogen for ISOM is supplied from the net gas compressor third stage discharge of Octanizingunit. The injection point of purified hydrogen is at the discharge of the recycle gas compressor.

Composition and specifications of the hydrogen is listed below:

| Table 3- Make Up Hydrogen Specification * From Octanizing |         |       |  |  |  |
|---|---------|-------|--|--|--|
| Composition, mol% Design Data Actual Data                 |         |       |  |  |  |
| Hydrogen  | 94.49   | 94.84 |  |  |  |
| Methane   | 2.02    | 1.86  |  |  |  |
| Ethane  | 2.15    | 1.63  |  |  |  |
| Propane   | 0.83    | 1.06  |  |  |  |
| N-butane  | 0.16    | 0.2   |  |  |  |
| I-butane  | 0.18    | 0.29  |  |  |  |
| C5+   | 0.17    | 0.14  |  |  |  |
| Total   | 100     | 100   |  |  |  |
| Viscosity ,cp   | 0.01032 | •••   |  |  |  |

## **5-2 Products Specification**

There are two primary products from the ISOM Unit, isomerate product and Stabilized LPG which are routed to storage tanks. In addition, off gas from Deethanizer and Stabilizer is sent to the refinery fuel gas header.

5-2-1 Isomerate
Specifications of product of ISOM unit (isomerate) are as follows:

| Table-4 Isomerate properties * |             |             |  |
|--------------------------------|-------------|-------------|--|
| Properties                     |             |             |  |
| Composition Data wt%           | Design Data | Actual Data |  |
| N-C4                           | 0           | 0.06        |  |
| Neopentane                     | 0           | 3.18        |  |
| Isopentane                     | 25          | 18.08       |  |
| N-C5                           | 1           | 12.49       |  |
| 2,2DMC4                        | 21          | 1.86        |  |
| CC5                            | 7           | 1.59        |  |
| 2,3DMC4                        | 7           | 4.67        |  |
| 2MC5                           | 22          | 17.80       |  |
| 3MC5                           | 10          | 9.26        |  |
| N-C6                           | 2           | 8.11        |  |
| 2,2DMC5                        | 0           | 0.38        |  |
| MCC5                           | 2           | 6.99        |  |

محل مهر خریدار:

محل مهر فروشنده:

| 2,4DMC5                      |              | 0          | 0.45  |
|------------------------------|--------------|------------|-------|
| 2,2,3TMC4                    | 0            |            | 0.09  |
| Benzene                      | 0.13         |            | 0.00  |
| 3,3DMC5                      |              | 0          | 0.29  |
| CC6                          |              | 2          | 4.02  |
| 2MC6                         |              |            | 1.77  |
| 2,3DMC5                      |              | 0          | 0.75  |
| 1,1DMCC5                     |              | 0          | 0.32  |
| 3MC6                         |              | 0          | 2.49  |
| cis-1,3DMCC5                 | 0            |            | 0.43  |
| trans-1,3DMCC5               |              | 0          | 0.43  |
| 3EC5                         |              | 0          | 0.21  |
| Trance-1,2DMCC               | 5 0          |            | 0.63  |
| N-C7                         |              | 0          | 1.34  |
| MCC6                         |              | 0          | 1.88  |
| EthylCC5                     |              | 0          | 0.26  |
| Molecular<br>Weight(kg/kmol) | 8            | 0.89       | 82.56 |
| RON                          | Guarantee 86 |            |       |
| MON                          | Expected 85  |            | -     |
| <b>Benzene Content</b>       | 0.1 vol%     |            | Nil   |
| RVP                          | Max 80 kPa   |            | 77    |
| YIELD                        | Guarant      | tee 92 wt% | 95    |

# 5-2-2 Stabilizer Deethanizer off Gas

The off gas from Stabilizer and Deethanizer will be directly routed to the refinery fuel gas header.

Flow rates and characteristics of the off gas are presented as follows:

| Table- 5 Stabilizer Deethanizer Off Gas Specification * |      |       |  |  |  |
|---|------|-------|--|--|--|
| Properties Design Data Actual run                       |      |       |  |  |  |
| Composition, mol%                                       |      |       |  |  |  |
| Hydrogen  | 14.9 | 14.55 |  |  |  |
| Methane   | 10.3 | 8.46  |  |  |  |
| Ethane  | 24.7 | 64.96 |  |  |  |

محل مهر خریدار:

محل مهر فروشنده:

| Propane                   | 42.1    | 10.98 |
|---------------------------|---------|-------|
| I-butane                  | 5       | 0.888 |
| N-butane                  | 2.9     | 0.148 |
| C5+                       | 0.0     | 0.06  |
| Total                     | 100     | 100   |
| Viscosity, cP             | 0.00956 | •••   |
| Molecular Weight, kg/kmol | 32.7    | •••   |
| Flowing Density, kg/m3    | 6.24    | •••   |

## 5-2-3 LPG Product

| Table- 6 LPG Product Specification * |             |            |  |  |
|--------------------------------------|-------------|------------|--|--|
| Composition mol%                     | Design data | Actual run |  |  |
| Hydrogen                             | 0           | 0          |  |  |
| Methane                              | 0           | 0          |  |  |
| Ethane                               | 0.0145      | 0.89       |  |  |
| Propane                              | 47.45       | 40.874     |  |  |
| I-butane                             | 25.54       | 36.596     |  |  |
| N-butane                             | 26.65       | 11.038     |  |  |
| I-pentane                            | 0.043       | 7.228      |  |  |
| N-pentane                            | 0.29        | 2.456      |  |  |
| Total molar flow rate (kmol/hr)      | 68.91       |            |  |  |
| Viscosity (cp)                       | 0.11666     | •••        |  |  |
| Molecular Weight (kg/kmol)           | 51.51       | •••        |  |  |
| Flowing Density(kg/m3)               | 514.5       | 555        |  |  |

\*<u>Difference between Design and Actual condition due to changing in crude oil feed, Suppliers must take samples from Isomerization FreshFeed,NC6 Recycle from Deisohexanizer column and shall analyze it by their laboratory.</u>

# 5-3 Design and operating conditions:

| Table-7Main Operation of Isomerization Unit |                     |               |                                     |                       |               |
|---|---------------------|---------------|-------------------------------------|-----------------------|---------------|
| Item  | Design<br>Condition | Actual<br>Run | Item                                | Design Condition      | Actual<br>Run |
| Fresh Feed Rate,m <sup>3</sup> /h           | 56.31*              | 80            | Reactor Inlet<br>Temperature, °C    | 220(SOR)/270(EOR)     | 240           |
| Reactor Feed (Gas), m3/hr                   | 3289                | •••           | Max. Reactor Delta T, °C            | 30                    | 24            |
| LHSV,h <sup>-1</sup>                        | 2                   | 1.4           | Reactor Outlet<br>Temperature, °C   | 250(SOR)/<br>290(EOR) | 264           |
| H2/HC Ratio,mol/mol                         | 1:2 (normally 1.05) | 1.1           | Recycle Gas Compressor (C-3301 A/B) |                       |               |
| Hydrogen Make<br>up,Nm3/h                   | 6214                | 2500          | Suction Pressure, barg              | 21.7                  | 22.5          |
| Recycle Gas<br>Flow,Nm <sup>3</sup> /h      | 21770               | 22500         | Discharge Pressure,<br>barg         | 29.8                  | 27.3          |
| Recycle Gas H2<br>Purity, mol%              | 82.5                | 93.67         |                                     |                       |               |
| Make-up Gas H2<br>Purity, mol%              | 94.49               | 95.16         |                                     |                       |               |

# **5-3 Catalyst Loading:**

| Table 8-Catalyst loading |                                    |  |  |
|--------------------------|------------------------------------|--|--|
| Reactor                  | Volume of Catalyst, M <sup>3</sup> |  |  |
| R-3301                   | 60 (max)                           |  |  |

# **5-4 Isomerization Heater:**

| Table 9- Isomerization Heater |                      |                              |  |
|-------------------------------|----------------------|------------------------------|--|
| Heater                        | Max Duty ,<br>Kcal/h | Max Outlet<br>Temperature °C |  |
| H-3301                        | 3.2*10^6             | 290                          |  |

<sup>\*</sup>This amount of feed is based on design condition of the unit. RON & yield of the product for minimum 80 m³/h(12076 BBL/day) should be calculated and guaranteed by catalyst suppliers.

## **5-4 Inlet Pressure of Reactor:**

| Table 10- Inlet Press. of Reactors , kg/cm <sup>2</sup> |      |  |  |
|---|------|--|--|
| Design  |      |  |  |
| R-3301  | 25.8 |  |  |

## **Section 6: Catalyst Performance**

## 6.1 Catalyst Requirement:

Catalyst type and quantity must meet the following requirements:

- 1. Catalyst to handle fresh feed rate as mentioned in Section 5-1 and under actual operating condition and Operating Constraints (section 7) the guaranteed items of table 11 shall be meet.
- 2. Catalyst offered should have proven commercial performance of minimum oneyear in operation.

# **6.2 Format for submission of yield guarantee:**

Based on RIPI design and guarantee for increase Light naphtha octane to 87 RON of Gasoline and below items should be guarantee with suppliers.

| Table-11 Guarantees Items         |           |  |  |
|-----------------------------------|-----------|--|--|
| Parameter                         | Guarantee |  |  |
| RON of Product                    | ≥86       |  |  |
| Benzene content on product        | 0.1% vol  |  |  |
| RVP of product, KPa               | Max. 80   |  |  |
| Yield of Product, wt%             | Min 92    |  |  |
| Total life of Catalyst(min), year | 6         |  |  |

# **6.3 Catalyst life Guarantee:**

The catalyst should be designed to meet the guaranteed quality, product yield, RON and specifications as per section 10 for a minimum period of 6 years operation while processing at feed specification as per section 5-1. Penalties as per section 11 will be applicable if the above is not met.

## 6.4 Performance Guarantee Test Run:

- 1-For establishing the above performance guarantees, test runs will be conducted either with design feed stock or feed stock having similar characteristics as those of design feed stocks. The performance guarantee test run for catalyst will be conducted within 6 months from the date of introduction of fresh feed after catalystloading.
- 2. The catalyst will be accepted by IKORC only if the guarantees specified by the vendor & IKORC have been met in the PGTR (Performance Guarantee Test Run). Otherwise penalties shall be applicable as per the section 11.
- 3. Catalyst supplier shall provide details, any procedures, special conditions required for conducting performance guarantee run. The analysis obtained from IKORC laboratory shall be considered as final. These methods shall be in accordance with normal practice. (No third party analysis is envisaged).
- 4. The test run shall commence when the unit is operating under stable conditions and shall be conducted for a period of 72 to 168 consecutive hours based on feed availability. Based on mutually agreed and jointly collected measurements during the test run, Catalyst supplier and IKORC shall evaluate the results of the test run to confirm conformity with the performance guarantees.

# 7 Operating Constraints

Below operating constraints of ISOM unit to be considered by vendor while designing the catalyst and providing guarantees.

- 1. Max. Charge Heater Tube Skin Temp. is 520 °C
- **2.** Maximum design heater outlet temperature is 270°C (End Of Run) (inlet temperature of R-3301)
- 3. Max. skin temp. of reactor at normal pressure 400 °C
- **4.** Maximum recycle gas actual flow is 21.77 KNM<sup>3</sup>/hr.
- 5. Maximum C7+ content for design shall be 8.0wt% on total feed

# 8 Scope of services:

Vendor shall provide the following services:

محل مهر خریدار:

محل مهر فروشنده:

- 8.1 Scope of Supply & Services
- i) Supply of necessary catalyst.
- ii) In price bid, the vendor has to quote total catalyst cost CFR bases.
- iii) Vendor should assist by deputing expert during catalyst loading, start-up assistance and Performance Guarantee Test Run activities. IKORC requires approximately 10 days on site service (24 hrs basis) as part of catalyst proposal i.e.3 days round the clock backup for catalyst loading and 7 days for start up and Test Run. Subsequent to the catalyst loading, vendor shall go back and come again during the start up. Above services must include all the travels, boarding, lodging, transport and miscellaneous allowances at vendor's scope. Vendor shall submit detailed catalyst loading, start-up and PGTR reports immediate after each activity. Time spent during transit will not be considered by IKORC.
- iv) In case IKORC requires more than 10 days vendor's service for this activity, vendor to quote per diem rates in price bids for services needed at site, which willnot be considered for evaluation of offers.
- v) Vendor has to certify and sign various stage wise documentary clearances during catalyst loading and reactors box up after inspection.
- vi) Catalyst supplier shall also provide a certificate of worthiness after the successfulcompletion of the catalyst loading. (Prior to first start up with the catalyst).
- vii) Vendor should provide operating parameters for other modes of operations (design & check cases).
- viii) Vendor shall provide periodic evaluation of catalyst performance on quarterly basis for ISOM. unit and offer technical assistance for trouble shooting arising in the unit till the catalyst is in use even after the guarantee period exceeds. Necessary data enabling the above will be furnished by IKORC.
- 8.2 Data / Documents to be submitted with the offer

Following information shall be submitted as a part of the technical offer (as per the following table format, Table - 12):

- a. Minimum Information to be furnished in the Technical Proposal is defined in thissection. Metric system of units shall be followed for all information.
- b. Catalyst wise: Name, Type, size, Density, Average bulk density,wt% metal of content, crushing strength, surface area, pore volume, Attrition loss, Crushing Strength, Loss on Ignition, the properties of catalyst with their standard method of measurement.

محل مهر خریدار:

- c. Catalyst supplier shall submit all the details and technical information including data with respect to Process Guarantees, duly signed and complete in all respects, along with the offer.
- d. Catalyst supplier to provide both the estimated values and guaranteed values at SOR and EOR.
- e. Catalyst supplier shall provide necessary procedure and loading diagram for theloading of catalyst in ISOM's reactor.
- f. Catalyst supplier to provide information on the following key operating parameters at SOR/EOR, as a minimum, in the proposal for all cases.
- \*Overall mass balance
- \*Reactor yield
- \*Temperature/Pressure at inlet and outlet of the Reactor
- \*Pressure drop across the Reactor
- \*Weighted Average Inlet Temperature (WAIT)
- \*Weighted Average Bed Temperature (WABT)
- \*The Recycle gas to oil ratio (H<sub>2</sub>/HC)
- \*C4+ Recovery Yieldwt.(%)
- \*C5 Activity wt.(%)
- \* C6 Activity wt.(%)
- g. As the vendor will specify SOR / EOR inlet, WAIT& WABT temperature, they will specifycatalyst deactivation rate at the design charge for the design feed.
- h. Vendor must quote catalyst quantity as packed basis in kg unit and mention volume in M<sup>3</sup> unit.
- i. Catalyst should be able to handle turndown with fresh feed at 50% of design.
- j. Precautions, emergency procedures to be followed during start-up / normal operation / upsets / turnarounds.
- k. Information regarding catalyst poisons.
- l. Catalyst packing, handling, storage, loading & unloading procedure.
- m. Detailed Catalyst Performance monitoring calculations/procedure.
- n. Catalyst reaction chemistry.
- o. Reference list of units where the catalyst has been in operation. Catalyst without proven one year commercial experience is not acceptable.
- p. All necessary technical information or the operating parameters that affect thecatalyst performance i.e. SOR & EOR conditions with respect to temperature, temperature rise, pressure drop, product yield, product quality etc.
- q. Signed Statement of Deviations as per the Tender documents.

- r. Vendor to note that catalyst will be loaded at a time determined by IKORC Guarantees will hold from the time whenever feed is introduced for the first time.
- s. Vendor to provide catalyst technical details/ Material Safety Data Sheet &manufacturers specification with the bid documents / Manufacturers certificate of analyses incorporating all properties given in the specifications for each batchsupplied.
- t. Catalyst to be packed suitably in steel drums on heavy-duty pallets.
- u. Vendor to indicate the estimated variation in inlet Temp. WABT, WAIT, H2/HC, C4+ Recovery Yield wt (%), C5 Activity wt. (%), C6 Activity wt.(%) and product qualities with respect to change in design case feed properties.
- v. Vendor to provide their catalyst deactivation details/WABT (WAIT) curve with respect to time for design case.
- w. Vendor to mention the list of documents required by vendor from IKORC at various stages.

All of the following items should be included in the technical offer clearly:

| MANUFACTURE COMPANY NAME  FACTORY ADDRESS & E-MAIL         |                     |      |
|--|---------------------|------|
|  |                     |      |
| FACTORY ADDRESS & E-MAIL                                   |                     |      |
|  |                     |      |
| CATALYST CHARACTERISTICS                                   | UNIT                | DATA |
| SOR TEMPERATURE @ 87 RON                                   | °C                  |      |
| EOR TEMPERATURE @ 87 RON                                   |                     |      |
| H <sub>2</sub> / HC mol. RATIO (MIN)                       | Mol/mol             |      |
| TOTAL LIFE   | year                |      |
| NO OF REGENERATION   |                     |      |
| C4+ RECOVERY YIELD   | wt. (%)             |      |
| C5 ACTIVITY  | wt%                 |      |
| C5 ACTIVITY  | wt%                 |      |
| BENZENE CONTENT IN ISOMERATE                               | vol%                |      |
| CATALYST PHYSICAL PROPERTIES*                              | •                   |      |
| SHAPE  |                     |      |
| DIAMETER   | mm                  |      |
| SURFACE AREA   | m <sup>2</sup> /gr  |      |
| PORE VOLUME  | cm <sup>3</sup> /gr |      |
| BULK DENSITY   | kg/m <sup>3</sup>   |      |
| CRUSHING STRENGTH  | N                   |      |
| ATTRITION LOSS   | wt%                 |      |
| LOI @ 900°C, 6 hr  | wt%                 |      |
| CATALYST CHEMICAL PROPERTIES*                              |                     |      |
| ACTIVE METAL CONTENT                                       | wt%                 |      |
| NITROGEN POISON LEVEL                                      | ppm wt              |      |
| SULPHUR POISON LEVEL                                       | ppm wt              |      |
| WATER CONTENT POISON LEVEL ppm wt                          |                     |      |
| TECHNICAL SERVICES (INCLUDING TRAINING AND TECHNICAL SUPPO | ORT)                |      |
| PERFORMANCE GUARANTEE**                                    |                     |      |
| USER REFERENCE LIST(COMPANY NAME & COUNTRY & YEAR & ADDR   | ESS )***            |      |

<sup>\*</sup>Third party inspection certificate of the catalyst properties and delivery contents. The third party company must be approved by the refinery (IKORC) and all the

expenses of site visit, sampling and catalyst tests, before delivery to be included in the catalyst price.

\*\*Catalyst supplier shall stand guarantee for yield, product specification, RON of product, Benzene content on product 0.1%vol throughout the life of catalyst.

\*\*\*If the suppliers do not submit the consumers list, removed from the tender and the bid will not be accepted.

## 9 Evaluation Criteria

9.1 The commercially offer will be equal with the following formula (Table - 13) and each items score (Table 14):

```
L = (100 * C) / (100 - (i*(100 - t)))
```

L = equal price

C = offer price

t = technical privilege (for accepted must be <math>t > 70)

i = coefficient effect (for catalyst i = 0.4)

| Tend  | er :ISOM Catalyst   | Tender NO.:RND-98182       | 25-MY       |                        |               |
|-------|---|----------------------------|-------------|------------------------|---------------|
| No.   | Criterion of technical assessment   | Weight percent             | Specia<br>1 | Description of details | Attached      |
| 1     | OPERATING COST  | 15                         |             |                        |               |
| 2     | LIFE OF CATALYST  | 20                         | *           |                        |               |
| 3     | PRODUCTIVITY OF CATALYST  | 50                         | *           |                        |               |
| 4     | TECHNICAL SUPPORT   | 5                          |             |                        |               |
| 5     | REFERENCE LIST  | 10                         | *           |                        |               |
| NO.   | Description of details  |                            |             |                        | Privilege     |
| 1     | OPERATING COST  |                            |             |                        |               |
|       | OPERATING COST including:1) inlet Re  | eactors Temp. 2) H2/HC F   | Ratio       |                        | Attached form |
| 2     | LIFE OF CATALYST  |                            |             | -                      |               |
|       | Catalyst Life including:1)No of catalyst's regenerations2)Total Life                          |                            |             |                        |               |
| 3     | PRODUCTIVITY OF CATALYST  |                            |             |                        |               |
|       | Quality & Productivity:1) RON of Isomerate2)C4+ Yield3) C5 Activity wt% 4) C6 Activity Attach |                            |             | Attached forn          |               |
| 4     | TECHNICAL SUPPORT   |                            |             | •                      |               |
|       | Technical Consulting: 1 ) Technical Suppo   | rt                         |             |                        | Attached form |
| 5     | REFERENCE LIST  |                            |             | •                      |               |
|       | provide references regarding successful an  | d satisfactory performance | e           |                        | Attached form |
| Oblig | gations   |                            |             | •                      |               |
| No.   | Description   |                            |             |                        |               |
| 1     | Guarantee of Section 10   |                            |             |                        |               |
| 2     | Visit of vendors Factory at time of product   | tion                       |             |                        |               |
| Expl  | anation:  |                            |             |                        |               |

1- technical privilege is 70 (t > 70)

min

2- Coefficient effect for catalyst i = 0.4

- 3- Special criteria: the criteria that if not get fully privilege, offer not acceptable
- 4- The commercially offer must be equal with the following formula

L=(100\*C)/(100-(i\*(100-t)))

L = equal price

C = offer price

t = technical privilege (for accepted must be <math>t > 70)

Table – 13 (Selection Criteria)

Table – 14 (technical privilege form)

| Technical privilege :Attached form for ISOM Catalyst |                   |                                      |   |  |
|--|-------------------|--------------------------------------|---|--|
| OBJECTIVE  | EFFECTIVENESS (%) | SUB.OBJECTIVE                        | EFFECTIVENESS<br>BASED ON OBJECTIVE (%) |  |
| OPERATING  | 15                | INLET TEMPERATUR (SOR/EOR)           | 40                                      |  |
| COST   | 13                | H <sub>2</sub> /HC                   | 60                                      |  |
| CATALYST   | 20                | GUARANTEED CYCLE LENGTH (TOTAL LIFE) | 90                                      |  |
| LIFE   |                   | NO.OF REGENERATION                   | 10                                      |  |
|  | 50                | C4+ yield WT%                        | 10                                      |  |
| PRODUCTS   |                   | C5 Activity WT%                      | 8                                       |  |
| PRODUCTS   |                   | C6 Activity WT%                      | 2                                       |  |
|  |                   | OCTANE(X)BBL                         | 80                                      |  |
| TECHNICAL SUPPORT 5                                  |                   | TECHNICAL SUPPORT                    | 100                                     |  |
| REFERENCE<br>LIST                                    | 10                | REFERENCE LIST***                    | 100                                     |  |

<sup>\*\*\*</sup> If the suppliers do not submit the consumers list, removed from the tender and the bid will not be accepted.

9.2 Offer not meeting guarantees mentioned in the section 10 is liable to be rejected.

## 10 Guarantees

Catalyst supplied by the vendor shall be subjected to the following guarantee conditions:

IKORC expects following guarantees to be met by the catalyst vendor for fresh feed rate of 56.3 M<sup>3</sup>/hr. Minimum guarantees to be met for any feed specification within range mentioned in section 5-1and under actual operating condition and Operating Constraints (section 7) and the guaranteed items of table 11 shall be meet.

Materials shall be guaranteed against manufacturing defects, materials, workmanship and design for a period of first cycle life. Warranty for replacement of material / accessories should be provided free of charges at our premises. The above guarantee/warranty will be without prejudice to the certificate of inspection or material receipt note issued by us in respect of the materials.

#### 10.1 Minimum Yield Guarantees:

Yield must be  $\geq$  Min 92% by wt.& Benzene content max0.1%vol., However vendor has to specify the estimated yield.

10.2 Minimum Product Quality Guarantees:

Product (Isomerate) must meet following minimum requirement quality:

- i) RON  $\geq$  86
- ii) Aromatic Content of Gasoline, max0.1%vol

However vendor has to specify the estimated above qualities.

## 10.3 Turndown Guarantees:

The targeted guaranteed turndown ratio is 50% of design feed for the unit. The turndown test run shall be for a period of 48 hours on continuous basis of operation while producing on-specification products with design feedstock. As per IKORC prerogative, turndown capacity test run or minimum possible capacity test run shall be carried out. However, it will be carried out within 6 months of start up.

- 10.4 Pressure drop Guarantee:
- i. Catalyst supplier has to provide the estimated pressure drop.
- ii. Catalyst supplier has to give maximum Pressure drop guarantee in the reactors. Guarantee includes reactors internals also.
- 10.5 Catalyst life/Cycle length Guarantees:
- i) Cycle length shall be minimum 6 years at design feed.

**Notes:** 

i. As the Supplier/Vendor will specify SOR / EOR inlet temperature, WABT, WAIT temperature and pressure drop across the reactor, they shall specify catalyst deactivation rate/curve at the design case.

#### 11 Penalties

## 11.1 Product Quality:

Guaranteed Product quality has to be met for the range of feed specification mentioned in the section 5-1. In case of not meeting any of the products quality as guaranteed, penalty will be as follows

- i) For every 1 Octane Number (RON) decrease in product as guaranteed, 0.5% of total catalyst cost will be recovered.
- ii) For every 1% by wt decrease in yield as guaranteed, 0.5% of total catalyst cost will be recovered.
- iii) For every 0.1% vol of benzene in Isomerate product, 0.3% of total catalyst cost will be recovered.
- iv) For every 1 increase in RVP(Kpa)of product as guaranteed, 0.1% of total catalyst cost will be recovered

#### 11.2 Turndown:

In case of not meeting turndown criteria, 5 % of total catalyst cost will be recovered.

#### 11.3 Catalyst Properties:

- ii) For every 0.05% decrease in Pt content as guaranteed, 0.5% of total catalyst cost will be recovered.
- 11.4 Performance Bank Guarantee (PBG)

For the purpose of recovery of penalty, vendor has to provide performance bank guarantee of 10% of total catalyst cost.

11.5 Total Failure of Catalyst

For any one of the following reasons, the catalyst is treated as 'total failure',

- 1. SOR overall WAIT, WABT is 5 Deg C higher than quoted by the vendor in the tender.
- 2. Following yield and product quality guarantees conditions at design charge 56.88M<sup>3</sup>/hr and feed specification range mentioned in 5.1.
- i) Product yield is not achieved min 90 % by wt.
- ii) Product (Isomerate)RON is not achieved 84.
- iii)Benzene content in product more than 0.5 vol%
- 3.for 0.15% by wt decrease in Pt content as guaranteed.
- 4. Restricts the continued operation of the unit at 106.44 m³/hr(inlet of reactor) reasons attributable tocatalyst.

This will be assessed during Performance Guarantee Test Run (PGTR). If the catalyst is observed to be a 'Total Failure', Vendor will be given a maximum of onemonth from the last date of PGTR to correct the failure. Vendor will be allowed onemore PGTR at the end of maximum one month to prove the performance of catalyst. If second PGTR also proves to be unsuccessful and the catalyst is a 'Total failure', vendor has to reimburse the CFR cost of entire catalyst in the form of credit notevalid for a period of one year which will be used for any purchase made by IKORC from the same vendor during the period of validity. In case of no such purchasetransaction, IKORC will cash the credit note.

11.6 Catalyst Life/Cycle length Guarantees liability:

The catalyst life will be evaluated during the cycle length. For any reduction in the life, the vendor has to repay the money equivalent to the cost in accordance with the formula given below.

- i. If it fails within one year, cost equal to total catalyst cost.
- ii. If it fails after one year the value shall be calculated in accordance with the below formula.

Cost to repay =(G\*F-A)\*C/(G\*F)

Where

**G** = first cycle guaranteed life (5 years)

F = Design Feed (MT/year)

**C** = **CFRc** price of catalyst

A = Actual feed processed till failure (MT)

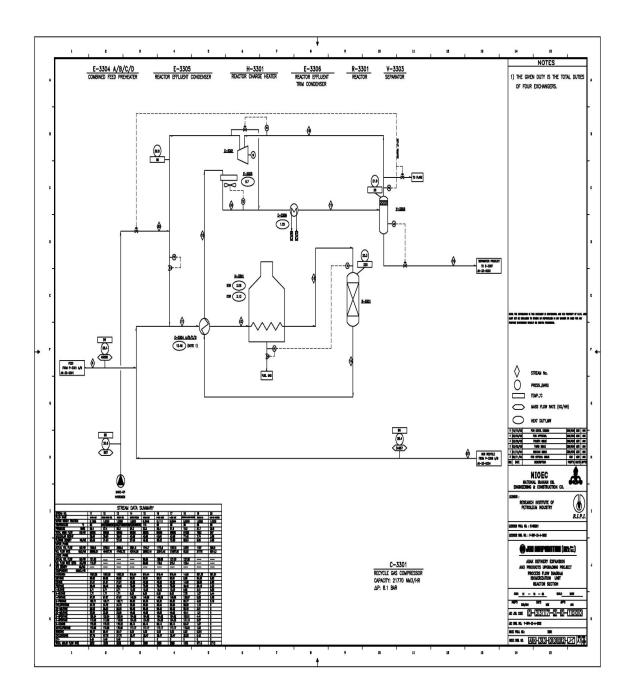
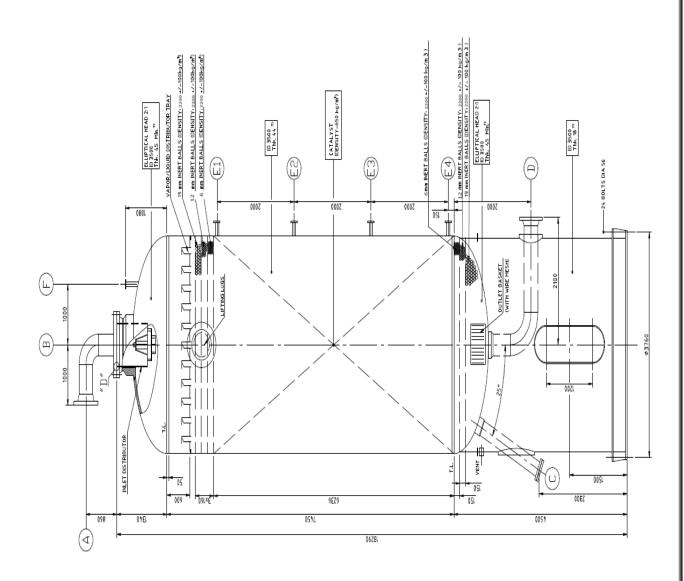


Figure 1-ISOM.unit Reactor



**Figure 2-ISOM Reactor Specification** 

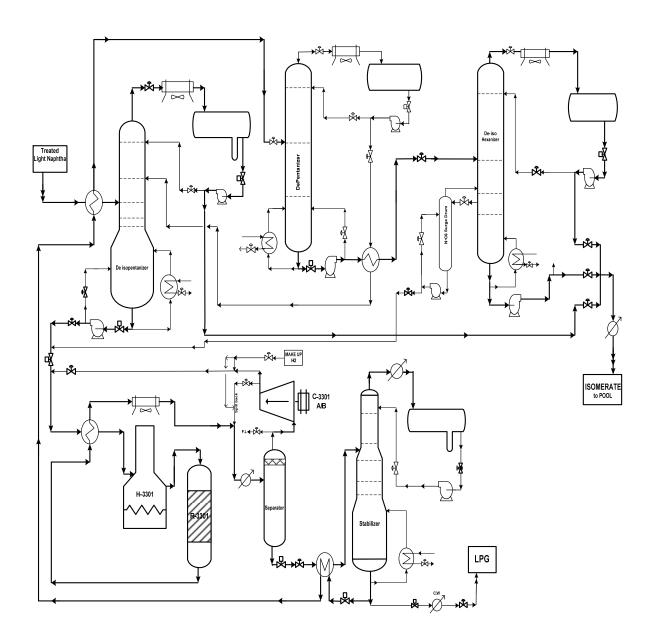


Figure 3-ISOM. unit